The role of protic solvent in asymmetric hydrogenation of methyl levulinate in the presence of a ruthenium-containing catalyst

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A comparative study of asymmetric hydrogenation and deuteration of methyl levulinate catalyzed by the Ru^{II}—(*S*)-BINAP—HCl system (BINAP is 2,2´-bis(diphenylphosphino)-1,1´-binaphthyl) in MeOH and MeOD was carried out. The results obtained suggest an important role of the protic solvent in the formation of catalytically active ruthenium complexes.

Key words: asymmetric catalytic hydrogenation, deuteration, hydrogen heterolysis, H/D exchange, ruthenium complexes, 2,2'-bis(diphenylphosphino)-1,1'-binaphthyl (BINAP), levulinic acid ester, chiral γ -valerolactone.

Earlier,¹ we have investigated asymmetric hydrogenation of levulinic acid esters catalyzed by the Ru^{II}—(S)-BINAP—HCl system (BINAP is 2,2′-bis(diphenylphosphino)-1,1′-binaphthyl). The resulting (S)- γ -hydroxy esters underwent *in situ* transformation into (S)- γ -valerolactone with up to 99% *ee*.

Here we studied the role of solvent in the aforementioned reactions with methyl levulinate (1) as a model substrate (Scheme 1).

Scheme 1

Me COOMe
$$H_2$$
 (D₂)/Ru^{II}—(S)-BINAP—HCI MeOD (MeOH)

1

 $R_{I_{I_{i_1}}}$
 O

2a,b

Experimental

R = H(a), D(b)

Commercial (S)-BINAP, (COD)Ru($H_2C(Me)C=CH_2$)₂ (COD is cycloocta-1,5-diene) (Acros), and D_2 and MeOD (pilot plant Prikladnaya Khimiya, St.-Petersburg) were used. Methyl levulinate was prepared from levulinic acid (Acros) according to a standard procedure.² Gaseous H_2 and D_2 were purified by passing through columns with a nickel—chromium catalyst and molecular sieves. All solvents were dehydrated before use. Catalytic hydrogenation of oxo ester 1 and analysis of

the reaction products were carried out as described in the preceding paper. Here the catalyst for the asymmetric hydrogenation and deuteration of oxo ester 1 was prepared *in situ* without isolating the intermediate complex [((S)-BINAP)RuCl₂].

Results and Discussion

Our experiments showed (Table 1) that the solvent nature strongly influences the rate and enantioselectivity of the catalytic hydrogenation of oxo ester 1.

The highest conversion and enantioselectivity were reached when the hydrogenation was carried out in water-free MeOH and EtOH (see Table 1, entries 1-3); the rate of the catalytic reaction in MeOH was appreciably

Table 1. Asymmetric catalytic hydrogenation of compound 1 in protic and aprotic media^a

Entry	Solvent	t/h	Conversion of compound 1	ee (S)
			%	
1	МеОН	3	100	99
2^b	EtOH	3	90	99
3^b	EtOH	5	100	99
4^b	Pr ⁱ OH	5	38	92
5	THF	5	<5	_
6	THF $-H_2O$ (9:1)	9c	74	67
7	CH ₂ Cl ₂	5	<5	_

^a Ru^{II}—(S)-BINAP—HCl; [1]/[Ru] = 200, [HCl]/[Ru] = 10, [1] = 1.7 mol L⁻¹, 60 atm (H₂), 60 °C.

^b Previous data¹ on the hydrogenation of ethyl levulinate in EtOH and isopropyl levulinate in PrⁱOH.

^c At 75 °C.

higher than in EtOH and $Pr^{i}OH$. In water-free aprotic solvents such as THF and $CH_{2}Cl_{2}$ (entries 5, 7), the reaction virtually did not occur under the same conditions. In aqueous THF (entry 6), the conversion of oxo ester 1 hydrogenated at 75 °C for 9 h was 74%. However, the reaction in this solvent was substantially less enantioselective (67% ee) than in alcohols, which is attributable to a change in the composition of the catalytic system in the presence of water. Earlier, 3 we have found that water deactivates the ruthenium catalyst in the deuteration of oxo ester 1 in aqueous 90% MeOH at 60 °C before complete conversion of oxo ester 1 into lactone 2 (at ~70% conversion).

The considerable acceleration of the reaction in protic solvents can be due to their role in the formation of catalytically active ruthenium complexes. To elucidate this issue, we performed a comparative study of Ru-catalyzed hydrogenation and deuteration of oxo ester 1 in MeOH, MeOD, and MeOH—MeOD.

A comparison of the kinetic curves in Fig. 1 shows that the catalytic hydrogenation with hydrogen in MeOH (curve *I*) and with deuterium in MeOD (curve *2*) have very close initial rates. This suggests that the kinetic isotopic effect of this reaction is absent or insignificant.

At the same time, one can assume that the heterolysis 4,5 of D_2 (H_2) is substantially facilitated in such a polar solvent as methanol. This is indicated by the data on the isotopic enrichment dynamics for lactone **2** during the catalytic reduction of oxo ester **1** with deuterium in MeOH and with hydrogen in MeOD (Fig. 2).

The dependences obtained suggest that the change in the isotopic composition of lactone 2 (ratio 2a/2b) is determined by the isotopic composition of the solvent (ratio MeOH/MeOD), regardless of whether hydrogen or deuterium is used as the reducing agent. For instance, in the reduction of oxo ester 1 with deuterium in MeOH (see

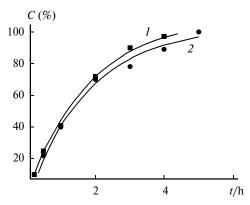


Fig. 1. Plots of the conversion (*C*) of methyl levulinate 1 vs. the hydrogenation time in MeOH (*I*) and the deuteration time in MeOD (2). The catalytic system is $(COD)Ru(H_2C(Me)C=CH_2)_2-(S)-BINAP-HCI;$ [1] = 1.7 mol L^{-1} ; [1] : [Ru] : [HCI] = 200:1:10; 60 atm $H_2(D_2)$; 40 °C.

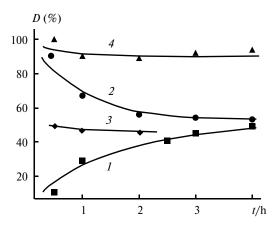
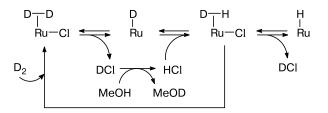


Fig. 2. Plots of the content of lactone 2b in the mixture of compounds 2a and 2b (D) vs. the reduction time in the reaction of methyl levulinate 1 with deuterium in MeOH (I), hydrogen in MeOH—MeOD (1:1) (J), and deuterium in MeOD (J). The catalytic system is (COD)Ru(H₂C(Me)C=CH₂)₂—(J-BINAP—HCl; [1] = 1.7 mol L⁻¹; [1] : [Ru] : [HCl] = 200:1:10; 60 atm D₂ (H₂); 40 °C.

Fig. 2, curve 1), lactone 2 contained ~10% deuterium in the γ -position 30 min after the reaction started (which corresponds to a ~20% conversion of compound 1) and ~50% deuterium after 4 h (90% conversion). When D_2 was replaced by H₂ and MeOH was replaced by MeOD, the dependence became opposite (see Fig. 2, curve 2): the deuterium content of the reaction product decreased from 100 to ~50% over the same period of time. In the reduction of oxo ester 1 by hydrogen in MeOH—MeOD (1:1), the contents of lactones 2a and 2b in the initial period of the reaction were also equal (see Fig. 2, curve 3). As expected, during the reduction of oxo ester 1 by deuterium in MeOD, the isotopic enrichment of product 2 in the γ -position changed only slightly (see Fig. 2, curve 4). Some decrease in it (from 100 to 90%) was due to the formation of MeOH as the result of partial H/D exchange between oxo ester 1 and MeOD.

The data obtained (see Fig. 2) can be explained by ruthenium-catalyzed H/D exchange⁶ between the reducing agent (D_2 or H_2) and the solvent (MeOH or MeOD) (Scheme 2), which occurs in parallel with the hydrogenation of oxo ester 1 and is much more rapid than the major hydrogenation (deuteration) reaction.

Scheme 2



In this case, a change in the MeOH/MeOD ratio during the catalytic reduction should correspondingly change the deuterium content of the catalytically active Ru-containing intermediates, which are in rapid equilibrium; in turn, their isotopic composition determines the ratio of lactones **2a** and **2b**. As noted above, the initial amounts of lactones **2a** and **2b** are equal at MeOH: MeOD = 1:1 (see Fig. 1, curve 3). This can be due to equal steady-state concentrations of hydrogen- and deuterium-containing ruthenium complexes. This fact is consistent with the absence of the kinetic isotopic effect in the catalytic reduction of compound **1** (see Fig. 1). Earlier, ^{7,8} intermediates of the types Ru(H₂) and Ru—H in equilibrium have been thought to participate in Ru-catalyzed hydrogenation of strongly enolized 1,3-diketones.

Based on the results obtained, one can assume that the Ru-catalyzed asymmetric hydrogenation of γ -oxo esters in protic organic solvents involves heterolysis of molecular hydrogen; a protic solvent facilitates this process and takes an active part in the formation of catalytically active ruthenium complexes that are in rapid equilibrium.

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